



Technical and Economic Assessment: Review and Proposed Directions

May 1-2, 2003

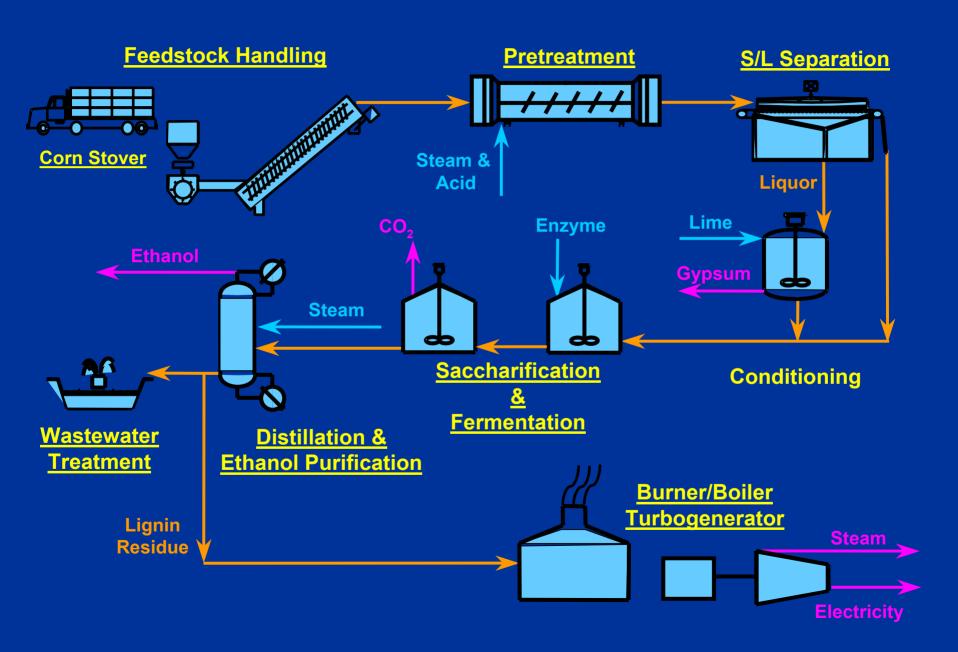
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Target-Case Report

- Design Report published in 2002 (NREL/TP-510-32438)
 - www.nrel.gov/docs/fy02osti/32438.pdf
 - ASPEN input code and Excel spreadsheets are available upon request
- Material and energy balances calculated with ASPEN+
 - 63 components tracked through 164 unit operation blocks
 - 82 control blocks
- Minimum Ethanol Selling Price (\$ per gallon ethanol)
 - Near-term estimates: Relative values between research options used to assist in guiding research
 - Long-term estimates: Absolute values used for policy analyses



Target Process Economics

Plant Size: 2200 tons (2000 MT) Dry Corn Stover/Day (Greenfield Site)
Corn Stover Cost: \$30/dry ton

Economic Parameter (Units, \$2000)	Value
Minimum Ethanol Selling Price (\$/gal)	\$1.07
Ethanol Production (MM gal/yr)	69
Ethanol Yield (gal/dry ton stover)	90
Total Project Investment (\$ MM)	\$197
TPI per Annual Gallon (\$/gal)	\$2.86
Minimum Sugar Selling Price (\$/lb)	\$0.056

Comparison of Target Parameters to NREL Measured Data

Parameter	Target	2002 Data	MESP Difference
Minimum Ethanol Selling Price (\$/gal)	\$1.07	\$2.42	\$1.35
Pretreatment Concentration	30%	19%	\$0.29
Pretreatment Monomeric Xylose Yield	90%	67.5%	\$0.12
Enzyme Cost (\$/gal)	\$0.10	\$0.64	\$0.54
Cellulose Hydrolysis Yield	90%	90%	\$0.00
Fermentation Sugars	All 5	Glucose / Xylose	\$0.12

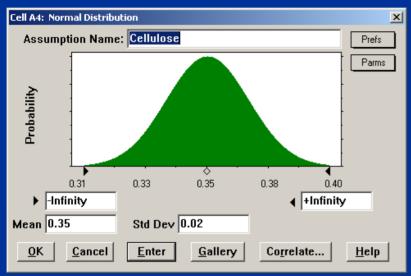
Pioneer Plant Costs

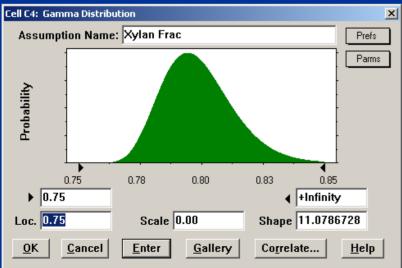
- Addresses technical and economic risk in the first-ofa-kind plant (Rand Corporation, 1981)
- Pioneer plant MESP: \$1.54-\$2.03 / gal
 - 44%-90% cost growth
- Systematic issues
 - Material and energy balances
 - Analytic chemistry
 - Impurities and their effects

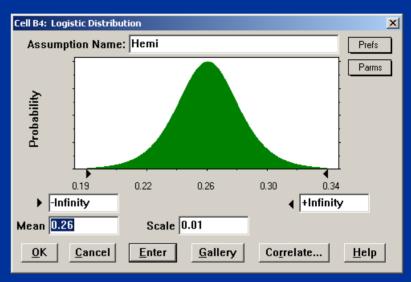
Monte Carlo Analysis

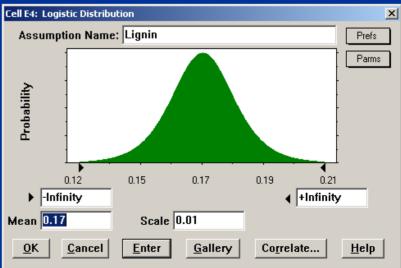
- Uses random numbers within defined functions to predict the uncertainty of modeled systems
 - Packaged software (e.g., Crystal Ball) makes it easier with Excel
- Used in the environmental, safety, business and other fields
- First analysis: Varying feedstock composition and high-impact process yields
 - Attempt to show potential variation in a working facility

Monte Carlo Analysis Parameters

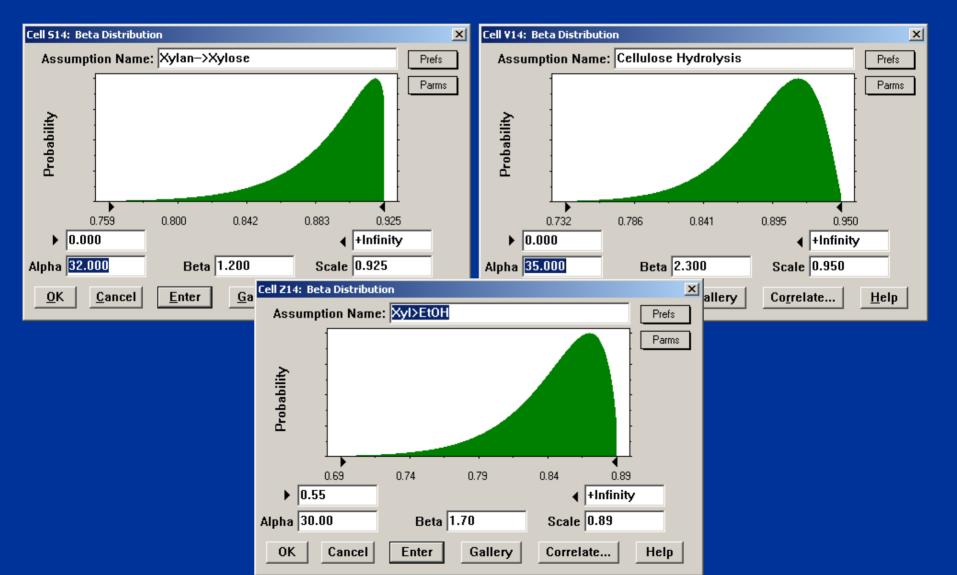






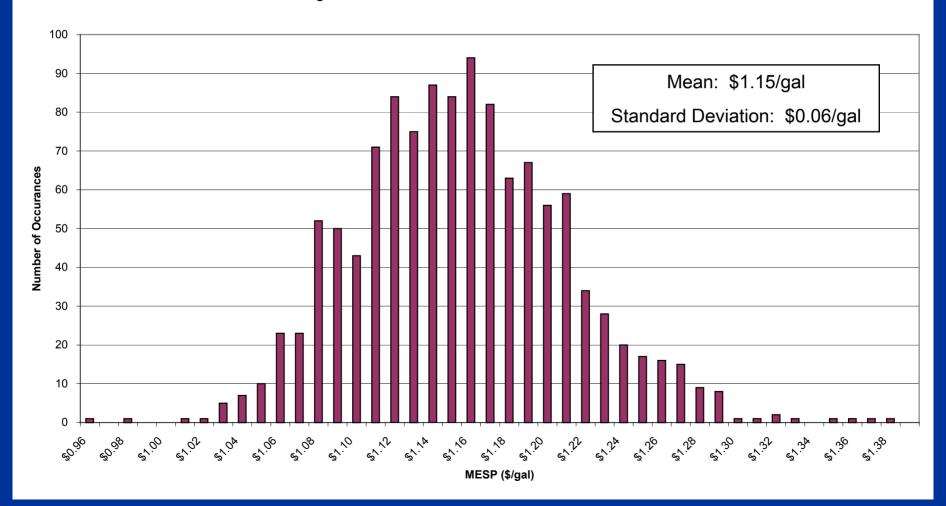


Monte Carlo Analysis Parameters



Monte Carlo Analysis Results

Histogram of MESPs for 1195 Monte Carlo Simulation Runs



Recommendations for Near-Term Work

- Legal and regulatory issues
 - Improve understanding of emissions issues and modify design to achieve emission regulations
- Technical feasibility and risk
 - Improve biomass handling and storage design
 - Links with biomass harvest strategy
 - Modify solid/liquid separation parameters to match pilotscale measurements
 - Improve modeling of conditioning (i.e., overliming) process area
 - Improve model's material balance by tracking additional components

Recommendations for Long-Term Work

- Technical feasibility and risk
 - Continue to track technology status
 - Link economic risk analysis to research error analysis
- Competitive advantage
 - Improve understanding of feedstock cost structure
- Strategic fit
 - Include kinetic models to develop an economic optimization tool
 - Develop LP models for biorefineries

Team Members

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